EVALUATION OF THE RATE OF CHANGE OF TRANSFER POTENTIALS IN POROUS SOLID BODIES

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A formula for calculating the potential diffusivity of energy in porous solid bodies has been obtained, which made it possible to express the velocity of propagation of the energy field in the form of a relation of the type of an equation of heat conduction with a constant coefficient. Under the same boundary conditions, the velocity of propagation of the energy field is intermediate in value between the velocities of propagation of the temperature and concentration fields.

The kinetics of the change of different transfer potentials (T, C, p_1, p_2) is usually described by equations of the type of equations of heat conduction with the corresponding kinetic coefficients a_h , $D_{s,liq}$, $a_m c_p \rho$, and K/g [1], and the time of propagation of the fields of the corresponding potentials, evaluated by the quantity l^2/a or l/v, can differ by several orders of magnitude [2]. In the latter case, there is no practical need to solve equations of combined transfer; it will suffice to solve an equation with a single potential whose propagation time is much larger than the propagation time of the other potentials. This problem remains unsolved in relation to enthalpy. It can be solved with the use of the energy characteristics of porous solid bodies [3].

As shown in [3], $W_{s,liq}$ is, by definition, the quantity of energy that must be expended in order that with a distance δ between holes in the liquid 1 mole (kg) of the substance overcome the resistance of the structure proper of the solid body and the liquid found in it (the solvent).

A traditional expression for the resistance to mass transfer in the steady state is δ/a . When the kinetics (the motion of the molecules) is considered in accordance with [4], we can write, taking into account the velocity of motion of the molecules δ/τ_{eq} ,

$$L_{\rm m} = \frac{\delta \frac{\delta}{\tau_{\rm eq}}}{W_{\rm s,liq}}.$$
 (1)

In accordance with [2; 4, p. 223], for a porous solid body saturated with a liquid, it can be assumed that $\delta^2/\tau_{eq} = 6D_{s,liq}$, and then

$$L_{\rm m} = \frac{6D_{\rm s.liq}}{W_{\rm s.liq}} \,. \tag{2}$$

By definition, L_m is the quantity of the substance (mole, kg) that is transferred a distance of 1 m at a velocity of 1 m/sec with an energy expenditure of 1 J.

The energy transfer is described by the expression

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$$L_{\rm e} = \frac{6D_{\rm s.liq}}{W_{\rm s.liq}} \, i \,. \tag{3}$$

1062-0125/00/7305-1108\$25.00 ©2001 Kluwer Academic/Plenum Publishers

UDC 66.015.23

All-Russia Scientific-Research Institute of Fats, St. Petersburg, Russia. Translated from Inzhenerno-Fizicheskii Zhurnal, Vol. 73, No. 6, pp. 1142-1144, November–December, 2000. Original article submitted October 19, 1999.

| Solid phase | Liquid phase (solvent) | <i>Т</i> , К | $D_{\text{s.liq}} \cdot 10^{12},$ m ² /sec | W _{s.liq} , kJ/kg | i, kJ/kg | $L_{\rm e} \cdot 10^{12}$, m ² /sec | $L_{\rm e}/D_{\rm s.liq}$ |
|-------------------------|------------------------|--------------|--|-------------------------------|-------------|--|---------------------------|
| Kernel of sov | Extractive gasoline | 293 | 0.24 | 24.4 | 200.3 | 11.82 | 49.2 |
| seeds | | 203 | 0.27 | 24.0 | 200.3 | 12.00 | 11 1 |
| secus | | 295 | 0.27 | 24.0 | 200.5 | 12.00 | ++.+ |
| | I I | | | | | | |
| | The same | 293 | 2.43 | 18.9 | 200.3 | 154.8 | 63.6 |
| Kernel of peanut | " | 309 | 3.08 | 19.5 | 231.3 | 219.0 | 71.4 |
| seeds | " | 325 | 3.74 | 20.9 | 262.7 | 282.0 | 75.6 |
| | " | 3/1 | 5 53 | 20.0 | 206.2 | 470.4 | 85.2 |
| | | 541 | 5.55 | 20.9 | 290.2 | 470.4 | 05.2 |
| | 1 | | | | | | |
| Microatomic sections of | | 298 | 0.71 | 22.2 | 209.9 | 40.26 | 57.0 |
| peanut seeds of | Commercial hexane | 298 | 0.72 | 22.2 | 209.9 | 40.86 | 57.0 |
| different thickness | | 298 | 0.63 | 22.5 | 209.9 | 35.28 | 55.8 |
| | | 208 | 0.34 | 23.6 | 200.0 | 18 12 | 53.4 |
| | | 298 | 0.54 | 23.0 | 209.9 | 10.12 | 55.4 |
| | 1 | | 1 | | | 1 | |
| Crumpled sunflower: | | | | | | | |
| without husks | Hexane | 323 | 0.21 | 32.3 | 259 | 10.2 | 48.6 |
| 5% husks | " | 323 | 0.05 | 30.2 | 259 | 2.58 | 51.6 |
| 10% busks | " | 373 | 0.05 | 30.2 | 259 | 2.58 | 51.6 |
| 10% husks | | 323 | 0.05 | 30.2 | 259 | 2.30 | 51.0 |
| 15% husks | | 323 | 0.06 | 29.7 | 259 | 3.12 | 52.2 |
| 25% husks | " | 323 | 0.21 | 26.7 | 259 | 12.24 | 58.2 |
| | | | | | | | |
| | Extractive gasoline | 328 | 9.1 | 25.2 | 269 | 583.2 | 64.2 |
| | Lind we dive gusseline | 328 | 15.2 | 23.8 | 260 | 1030.8 | 67.8 |
| | | 328 | 13.2 | 23.8 | 209 | 1030.8 | 07.8 |
| | | 328 | 17.3 | 23.0 | 269 | 1213.8 | 70.2 |
| | | 328 | 7.1 | 23.5 | 269 | 487.8 | 69.0 |
| | | | | | | | |
| | Dichloroethane | 328 | 6.4 | 26.9 | 269 | 384.0 | 60.0 |
| Damp soy petals | " | 328 | 15.4 | 22.3 | 269 | 1114.8 | 19.8 |
| of different | | 220 | 21.7 | 20.5 | 20) | 1709.2 | 70.2 |
| of different | | 328 | 21.7 | 20.5 | 269 | 1708.2 | 19.2 |
| thickness | | 328 | 16.8 | 20.0 | 269 | 1356.6 | 81.0 |
| | | | | | | | |
| | Extractive gasoline | 325 | 0.38 | 25.6 | 263 | 23.4 | 61.8 |
| | 2 | 325 | 0.30 | 26.1 | 263 | 18.12 | 60.6 |
| | | 229 | 2.50 | 20.1 | 260 | 107.4 | 76.0 |
| | | 328 | 2.39 | 21.2 | 209 | 197.4 | 70.2 |
| | 1 | | 1 | | | i. | ı I |
| | Trichloroethylene | 300 | 5.1 | 17.4 | 214 | 435.6 | 73.8 |
| | | 300 | 8.5 | 17.6 | 214 | 620.4 | 73.2 |
| | The same | 300 | 191 | 14 9 | 214 | 1645.8 | 964 |
| | The sume | 200 | 10.9 | 16.1 | 214 | 961.6 | 70.9 |
| | | 300 | 10.8 | 10.1 | 214 | 801.0 | 79.0 |
| ~ · | | | | a a <i>i</i> | | | |
| Soy grits | Extractive gasoline | 328 | 3.11 | 20.4 | 269 | 246.0 | 79.2 |
| | | | | | | 1 | |
| Grits of | The come | 200 | 0.65 | 24.2 | 260 | 42.0 | 66.6 |
| coriander waste | i ne same | 528 | 0.05 | 24.3 | 209 | 43.2 | 00.0 |
| | , I | | | | | | |
| Prepressed sunflower | | | | | | | |
| netal | Hexane | 323 | 16.1 | 22.3 | 259 | 1122.0 | 69.6 |
| Pettin | | | 1 | | | 1 | |

TABLE 1. Results of Calculation of the Potential Diffusivity of Energy

Since the chemical potential per unit volume of the substance is

$$\mu = \rho \left(\mu_0 + RT \ln C\right), \tag{4}$$

the material and energy fluxes expressed in terms of it will, respectively, be equal to

$$q_{\rm m} = L_{\rm m} \,\rho RT \frac{\partial}{\partial x} \left(\ln C \right) \,, \tag{5}$$

$$q_{\rm e} = L_{\rm e} \,\rho RT \frac{\partial}{\partial x} \left(\ln C\right)\,,\tag{6}$$

 $L_{\rm e}$ is an analog of the coefficients $a_{\rm h}$ and $D_{\rm s,liq}$; therefore, in the case where it is constant, we can write an equation for the velocity of propagation of the chemical potential:

$$\frac{\partial \mu}{\partial \tau} = L_{\rm e} \nabla^2 \mu \,. \tag{7}$$

Results of calculation of L_e are presented in Table 1. The data on $D_{s,liq}$ are taken from the works cited in [3], while *i* is taken from [5]. As is seen from the table, in the cases considered, the quantity L_e is intermediate between $D_{s,liq}$ and a_h [6], i.e., under the same boundary conditions the velocity of propagation of the energy field (the field of μ) in porous solid bodies is also intermediate in value between the velocities of propagation of the fields of *T* and *C*. This is natural, since μ is a function of *T* and *C*.

NOTATION

T, temperature; *C*, concentration; p_1 , unrelaxed vapor pressure; p_2 , hydrodynamic pressure of the liquid or the liquid mixed with the vapor (gas); a_h , thermal diffusivity; $D_{s,liq}$, diffusivity in the solid–liquid system; $a_m c_p \rho$, potential diffusivity of unrelaxed vapor pressure; a_m , potential diffusivity of mass transfer; ρ , density; c_p , heat capacity of the moist air in the porous body; *K*, filtration coefficient; *g*, free-fall acceleration; *a*, potential diffusivity (a_h , $D_{s,liq}$, etc.); δ , elementary displacement of a molecule; *v*, velocity of propagation of the field; *l*, dimension of a particle (radius of the sphere, half of the thickness of the plate); τ_{eq} , time of oscillation of a molecule about the equilibrium state in the liquid inside the porous body ("time of settled life"); *i*, enthalpy of the diffusing substance; L_e , potential diffusivity of energy; μ , chemical potential; *R*, gas constant; q_m , material flux; q_e , energy flux; μ_0 , chemical potential in the steady state; τ , current time; *x*, coordinate.

REFERENCES

- 1. A. V. Luikov and Yu. A. Mikhailov, Theory of Heat and Mass Transfer [in Russian], Moscow (1963).
- 2. V. V. Beloborodov, Inzh.-Fiz. Zh., 72, No. 1, 141-146 (1999).
- 3. V. V. Beloborodov, Inzh.-Fiz. Zh., 73, No. 2, 283-287 (2000).
- 4. Ya. I. Frenkel', *Kinetic Theory of Liquids* [in Russian], Leningrad (1975).
- 5. I. V. Molchanov, Technological Equipment for Fat-Processing Industries [in Russian], Moscow (1965).
- 6. A. S. Ginzburg (ed.), *Thermophysical Characteristics of Foodstuffs and Food Materials. Handbook* [in Russian], Moscow (1975).